

Original Article

STATISTICAL AND KINETIC STUDIES OF ACID PROTEASE BY *ASPERGILLUS* SPP. ISOLATED FROM SOIL CONTAMINATED WITH ABATTOIR WASTE

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ABSTRACT

Objective: Aim of the present investigation was to optimize the acid protease production from *Aspergillus* spp. through statistical method in solid state fermentation and to study the inhibitory enzyme kinetics.

Methods: To fulfill above mentioned aim, seven solid substrates were screened through using PBD (Plackett-Burman Design) and concentrations of three significant were determined by using one of the Response surface methodologies (RSM), Box-Behnken design (BBD). Inhibitory enzymatic effects were carried by using previously developed models.

Results: From PBD, wheat bran, soybean meal, and dried potato peel (DPP) were screened as major influencing nutritional factors for enzyme production. Better optimal values were determined by BBD as wheat bran: 8.841 g, soybean meal: 4.557 g, and DPP: 0.661 g with predicted protease activity as 817.83 U/g (± 44.047 U/g). Linear, interactive, and quadratic effects of aforesaid substrates on enzyme activity were formulated by quadratic model through multiple regression model (R^2_{Adj} : Adjusted R square = 94.78%; R^2_{Pre} : Predicted R square = 98.13%). Partial substrate inhibition to crude acid protease activity was notified with casein concentration higher than 0.4 mmol and inhibitory constant, K_N , was computed with previous developed mathematical models. Ratio of reaction rate constants, k_4/k_2 , was found to be 0.233 that had confirmed partial casein inhibition to enzyme velocity. Improved activity and kinetics of caseinolysis make amicable for industrial applications.

Conclusion: Quick optimization was performed with statistical methodology over conventional approach. Inhibitory enzyme kinetic studies were important for industrial applications of acid protease.

Keywords: Acid protease, Optimization, Statistical methodology, Casein inhibition, Reaction velocity

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INTRODUCTION

Proteases [E. C.3.4.21-25] catalyze proteolysis which are most industrially important hydrolases [1, 2]. Contribution of these enzymes to total enzyme sales is about 60% due to their exploitation in pharmaceutical, detergent, leather, and food industries [3, 4]. The increasing trend of microbial protease in pharmaceutical applications was summarized by [1]. Especially acid proteases from fungal species have promised applications in pharmaceutical, cheese, meat processed, baking, and soy sauce industries [5-7]. Moreover these are function as therapeutic agents in development of de clotting and anti-inflammatory, antimicrobial activities [5-7]. Mainly species of *Mucor*, *Aspergillus*, *Penicillium*, and *Rhizopus* are being capable of producing acid proteases [3, 8, 9].

Designing of suitable fermentation medium with economic concern is a challenge as it affects the product yield and it can be achieved through optimization techniques [10]. Several classical (OVAT: One variable at a time) and statistical methodologies are available for fermentation optimization [11]. In OVAT approach, one variable is changed by keeping others as constants which is a tedious method as it requires more number of experimental runs and ignores the interactions among selected parameters of fermentation [12, 13]. However, statistical methods establish a systematic relationship between input and output of fermentation to eliminate the drawbacks of classical approach [14, 15].

Substrate inhibitory studies are common in many enzymatic reactions as rate of reactions are inhibited by excess substrate which are crucial in the design of enzyme reactors and also in regulation of metabolic pathways [16-18]. Availability of literature on acid protease optimization and also on studies at substrate inhibitory level for enzymatic reactions is scanty. Therefore the present

investigation was performed to identify the significant solid substrates for acid protease production from fungi, *Aspergillus* spp. using PBD (Plackett-Burman design) and to find out the optimum combination of screened substrates through BBD (Box-Behnken design) in solid state fermentation (SSF). Further study was extended to analyze the casein inhibition on initial velocity of crude protease through various kinetic models.

MATERIALS AND METHODS

Materials

Wheat bran and soybean meal were obtained from local market. Potato peel was collected from kitchen waste and allowed to air dried. Remaining chemicals were of analytical grade (Hi-Media).

Screening of solid substrates

In the present work, Plackett-Burman design was summarized in table 1 and individual combination of fermentation medium was represented by each row. According to PBD design the fermentation media were prepared with composition of seven selected substrates. The frequencies of high (Coded as+1) level runs are same as that of low (-1) level runs (table-1). Then Erlenmeyer flasks with specified medium were moistened with 60% (v/w) salt mineral solution of composition: in (g/l) K_2HPO_4 1, KH_2PO_4 3, Mg_2SO_4 1, and $CaCl_2$ 0.1 and $ZnSO_4$ 0.01. Fungal spore Inoculum was prepared from the stock culture of *Aspergillus* spp. isolated from soil contaminated with abattoir waste [19]. Later sterilized medium was inoculated with 10% (v/w) fungal spore suspension. Then the contents of the flasks were mixed thoroughly and incubated at room temperature for 120 h (5 d) with an initial pH of 6.0. Crude protease was extracted by adding 50 ml of distilled water to flask, mixing at 150 rpm at room temperature for an hour. After incubation the dry weight of fungal biomass and

protease activity was performed [19]. Unit of protease was defined as liberation of one microgram of tyrosine from substrate per minute and the acid protease activity was expressed as U/g solid substrate. Protein content in the fungal filtrate was analyzed [20].

The regression analysis was employed to the best of experimental data through a first order linear model as follows:

$$Y_p = \beta_0 + \sum_{i=1}^7 \beta_i X_i \quad \text{----- (1)}$$

Where Y_p: Predicted protease activity, X_i: Coded settings for seven substrates, β₀: Model intercept, β_i: Linear coefficients of model

Optimization of significant substrates through Box-Behnken design

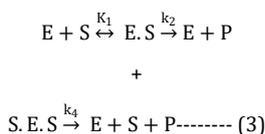
Based on PBD results, amounts of key factors wheat bran, soybean meal, and dried potato peel (DPP) were optimized by BBD which includes three levels as low (-1), center point ('0'), and high settings ('+'). Fermentation medium was prepared as per table 3 and SSF and analysis was carried as described above. Design matrix (table 3) consists of three blocks with each block corresponds to four rows and three central runs at the end in a total of 15 experiments. In the first block, wheat bran and soybean meal were kept at low and high levels that corresponds to 2²matrix while DPP is kept at its center value. In a similar way, soybean meal is at center point in the second block while wheat bran is made as center in third block. A second order polynomial equation, fitted to data by multiple regression procedure, resulted in quadratic model as follows:

$$Y = \beta_0 + \sum_{i=1}^3 \beta_i X_i + \sum_{i=1}^2 \sum_{j=i+1}^3 \beta_{ij} X_i X_j + \sum_{i=1}^3 \beta_{ii} X_i^2 \quad \text{----- (2)}$$

Y-Predicted response, X₁-Wheat bran, X₂-Soybean meal, X₃-DPP, β₀- Value of fitted response at the center point of the design, β_i-Independent terms, β_{ij}-Interaction coefficients, β_{ii}-Quadratic coefficients

Kinetics of casein inhibition

In order to study the enzyme activity as a function of casein amount, experiments were performed with substrate concentration range from 0.1 to 2.2 mmol. Resulted data were tried to fit to below mentioned mathematical models of substrate inhibition (SI) with the following reaction mechanism:



(Above reaction mechanism, Eq.3, was adopted from previous studies [16, 21, 22]).

Where [S]: Substrate concentration; E: Enzyme; P: Product

E. S: Enzyme-Substrate complex; S. E. S: Substrate-Enzyme-Substrate complex.

V: Velocity of reaction; V_{max}: Maximum reaction velocity

K₁ and K_N: Dissociation constants for E. S and S. E. S complexes

k₂ and k₄: Reaction rate constants

Model 1 (Andrew's model [21])

The assumption of rapid equilibrium yields

$$V = \frac{V_{max}[S]}{K_1 + [S] + \frac{[S]^2}{K_N}} \text{----- (4)}$$

At low substrate concentrations, $\frac{[S]^2}{K_N} \ll 1$, and inhibition effect was not observed and velocity was

$$V = \frac{V_{max}}{1 + \frac{K_1}{[S]}} \text{----- (5)}$$

At high casein concentrations, K₁/[S] << 1, the rate in this case was

$$V = \frac{V_{max}}{1 + \frac{[S]}{K_N}} \text{----- (6)}$$

Model II: (Adopted from [18])

$$\frac{(V_{max}-V)}{V} = \frac{[S](1 - \frac{k_4}{k_2})}{K_N + [S]\frac{k_4}{k_2}} \text{----- (7)}$$

RESULTS AND DISCUSSION

Current investigation was focused on easy way of the design of fermentation medium with inexpensive nutritional variables for optimization of extracellular acid protease production through SSF by *Aspergillus* spp. The use of quadratic response surface models makes the method much simpler than standard nonlinear techniques for determining optimal designs [10, 23].

Identification of influenced substrates through two-level PBD

Minimal and maximal response was observed as 54.12 and 307.30 U/g from selected carbon and nitrogen sources (table 1 and 2) through screening method. Discrimination between significant and non-significant substrates were based upon the calculated values of main effect and probability values (P-value) [24] which were summarized in table 2. Among the tested substrates, *P≤0.01 revealed that wheat bran (Main carbon source), soybean meal (Main nitrogen source), and DPP (Additional carbon source) induced microbial growth as well as biocatalyst activity. However, negativity in enzyme production was observed with corn flour as it was in fourth place therefore it could not select for response surface methodology (RSM).

The remaining substrates groundnut meal, rice flour, and cracked wheat were neglected for further optimization studies as *P>0.01. Same authors optimized several physical, chemical, and nutritional parameters for the same enzyme from the same fungal culture through OVAT and revealed that cracked wheat was the preferable main carbon source to wheat bran [25]. Comparison between OVAT and PBD revealed that wheat bran was the more effective carbon source when it was supplemented with various combinations of other substrates as it was missing with non-statistical method. Based upon observations of two approaches viz., OVAT reported by [25] and the present investigation, conventional approach had led to wrong conclusions as suggested by [6].

Table 1: Solid substrates with coded settings and actual concentrations (%w/w) with response of fermentation for PBD

Trial	Carbon and nitrogen sources							Observed Protease activity (U/g)
	X ₁ Wheat bran	X ₂ Cracked wheat	X ₃ Groundnut meal	X ₄ Soybean meal	X ₅ Corn flour	X ₆ Dried potato peel	X ₇ Rice flour	
R ₁	+1(10)	+1(10)	-1(0.5)	+1(5)	-1(2.5)	+1(1.0)	-1(0.5)	307.32
R ₂	-1(5.0)	+1(10)	+1(1.0)	-1(2.5)	+1(5)	+1(1.0)	-1(0.5)	61.76
R ₃	-1(5.0)	+1(10)	+1(1.0)	+1(5.0)	-1(2.5)	-1(0.5)	+1(1.0)	115.06
R ₄	+1(10)	-1(5.0)	+1(1.0)	+1(5.0)	+1(5.0)	-1(0.5)	-1(0.5)	160.56
R ₅	-1(5.0)	-1(5.0)	-1(0.5)	+1(5.0)	+1(5.0)	+1(1.0)	+1(1.0)	143.82
R ₆	+1(10)	+1(10)	-1(0.5)	-1(2.5)	+1(5.0)	-1(0.5)	+1(1.0)	81.40
R ₇	+1(10)	-1(5.0)	+1(1.0)	-1(2.5)	-1(2.5)	+1(1.0)	+1(1.0)	176.22
R ₈	-1(5.0)	-1(5.0)	-1(0.5)	-1(2.5)	-1(2.5)	-1(0.5)	-1(0.5)	54.12

*R1-R8 represented eight different fermentations; *Values in table-were represented as mean of two trials, *Amount of each substrate was measured in grams.

Table 2: Calculation of main effects using MS excel-7 and Identification of significant and non-significant substrates from results of PBD for biocatalyst production

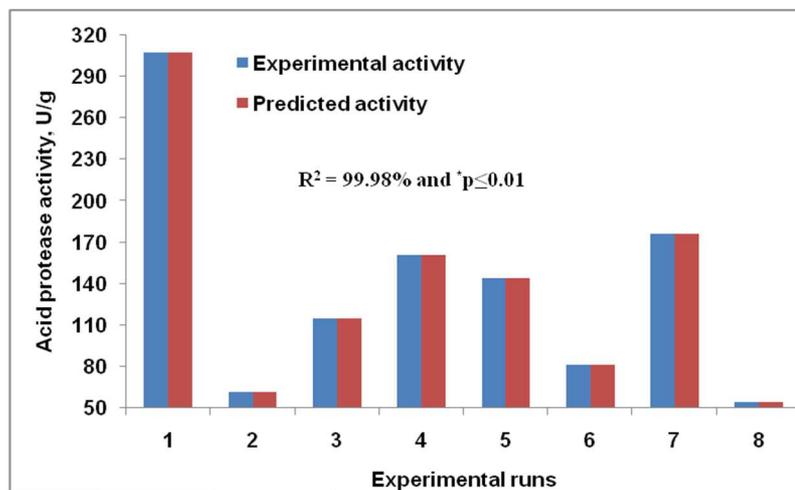
Factor	Main effect	Standard error	P value
Wheat bran (X₁)	43.84	7.50	<0.01 (Significant)
Cracked wheat (X ₂)	3.85	8.78	0.70 (Non-Significant)
Groundnut meal (X ₃)	-9.13	6.54	0.29 (Non-Significant)
Soybean meal (X₄)	44.15	7.50	<0.01 (Significant)
Corn flour (X ₅)	-25.64	7.50	<0.05 (Non-Significant)
Dried potato peel (X₆)	34.74	7.50	≤0.01 (Significant)
Rice flour (X ₇)	-8.41	7.00	0.35 (Non-Significant)

Fitness of experimental data to following proposed linear model for the present biocatalyst production was evaluated through regression analysis at 99% confidence level ($P \leq 0.01$) and it was formulated in Eq. (8)

$$Y_p = 137.53 + 43.84 X_1 + 3.85 X_2 - 9.13 X_3 + 44.15 X_4 - 25.65 X_5 + 34.75 X_6 - 8.41 X_7 \quad (8)$$

Predicted activity of biocatalyst, Y_p , was computed from Eq. (8) and the less deviation of predicted data from experimental activity was

observed since the regression coefficient was 99.88% (Fig.1). PBD could provide significant variables but not the optimal quantity of each substrate for optimum enzyme production as it ignores interactive effects of substrates as it had given an idea about potent nutritional variables from examined substrates.

**Fig. 1: Depiction of experimental and predicted acid protease activity using plackett-burman design of experiments**

Prediction of optimal combination through box-behnken design

Evaluation of screened nutritional factors at three levels (-1, 0,+1) was much useful in achieving the maximum productivity of protease. With BBD of keyfactors, the minimum and maximum protease

activities were observed as 121.59 and 807.83 U/g (table 3). Biomass prediction was estimated from Eq.10.

Production of enzyme solely was a function of growth of *Aspergillus* spp. so that the profile of fungal biomass was shown in fig. 2.

Table 3: Box-behnken design for three substrates with coded values with observed and predicted enzyme activity from *Aspergillus* spp. in SSF

Trial	Wheat bran X ₁	Soybean meal X ₂	Dried potato peel X ₃	Acid protease activity (U/g)	
				Mean experimental	Predicted
1	-1(5.00)	-1(2.50)	0(0.75)	109.08	121.59
2	-1(5.00)	1(5.00)	0(0.75)	213.26	237.77
3	1(10.0)	-1(2.50)	0(0.75)	525.4	500.94
4	1(10.0)	1(5.00)	0(0.75)	747.07	734.6
5	-1(5.00)	0(3.75)	-1(0.50)	119.08	140.83
6	-1(5.00)	0(3.75)	1(1.00)	339.21	280.57
7	1(10.0)	0(3.75)	-1(0.50)	687.05	745.75
8	1(10.0)	0(3.75)	1(1.00)	573.49	552.9
9	0(7.50)	-1(2.50)	-1(0.50)	417.28	383.11
10	0(7.50)	-1(2.50)	1(1.00)	271.31	317.53
11	0(7.50)	1(5.00)	-1(0.50)	565.72	541.17
12	0(7.50)	1(5.00)	1(1.00)	496.71	530.98
13	0(7.50)	0(3.75)	0(0.75)	807.83	807.83
14	0(7.50)	0(3.75)	0(0.75)	807.80	807.83
15	0(7.50)	0(3.75)	0(0.75)	807.80	807.83

*Values in above table were represented as mean of two trials, *Amount of each substrate was measured in grams, *R²_{Adj} (Adjusted R square) = 94.78%; R²_{Pre} (Predicted R square) = 98.13%

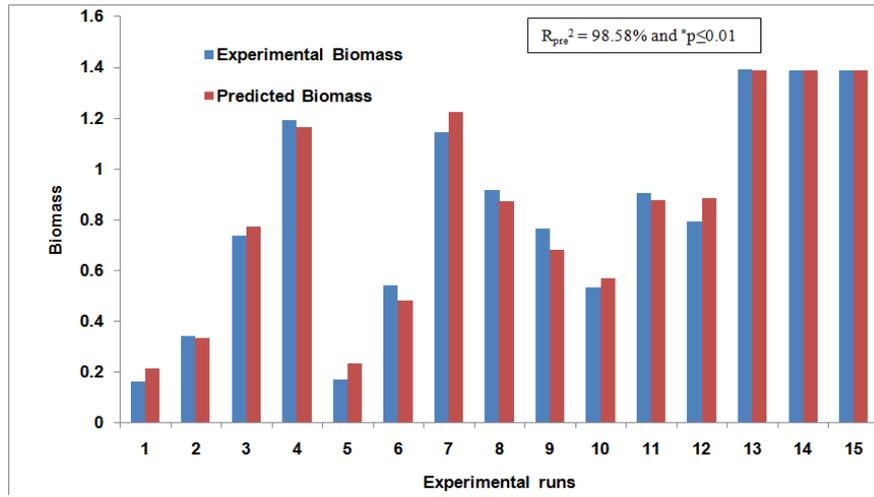


Fig. 2: Plot showing experimental and predicted mass of *Aspergillus* spp. with Box-Behnken approach

Scattered data obtained from 15 experimental runs was depicted in response surface plot in fig. 3. Surface plot fairly indicated a general increase in model response as concentrations of wheat bran and soybean meal increased from their center ('0') to higher

('+') values. Interactions among selected carbon and nitrogen sources were depicted in fig. 4 to 6 with respective slices of DPP (fig. 4a), soybean meal (fig. 5a), and wheat bran (fig. 6a) in three dimensional form.

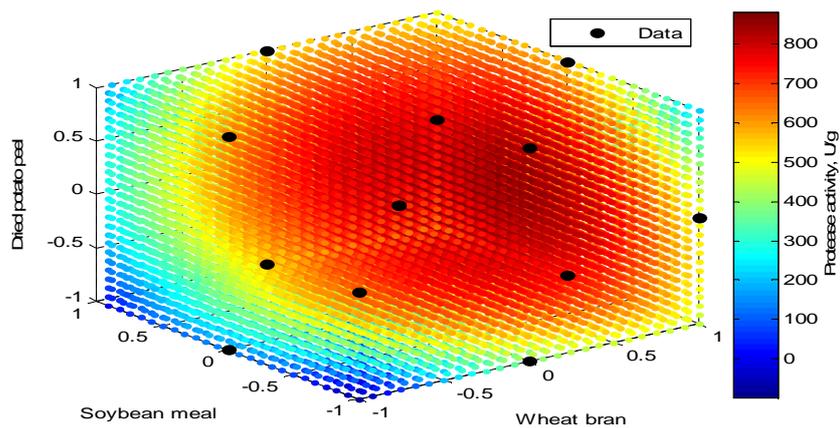


Fig. 3: Three dimensional plot depicting quadratic response surface model with three axes as wheat bran (5-10% w/w), soybean meal (2.5-5% w/w), and dried potato peel (0.5-1.0% w/w)

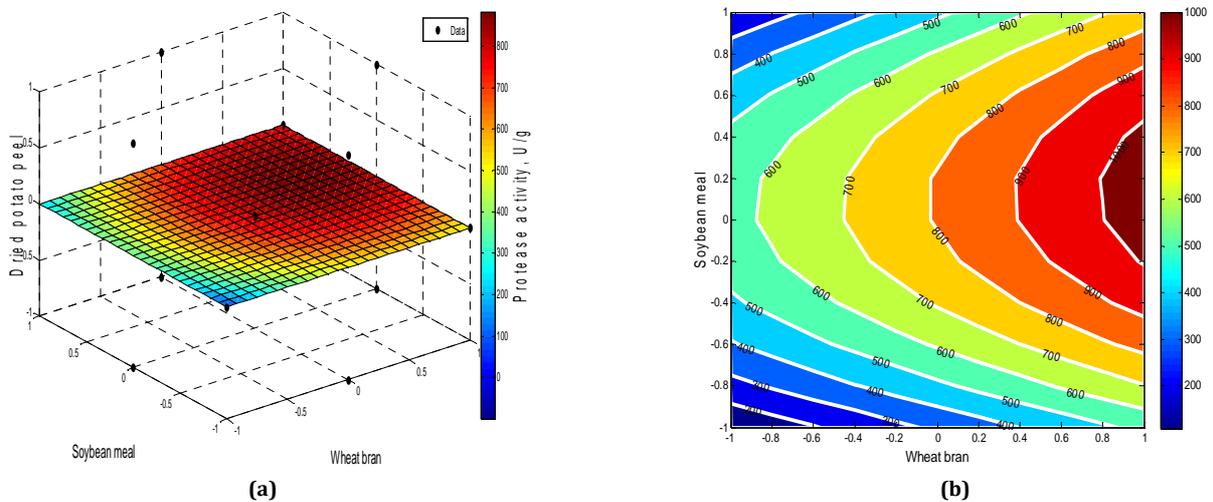


Fig. 4: Two-way interactions between wheat bran and soybean meal with 0.75% (w/w) of DPP, (a) Three dimensional plot and (b) Contour diagram with predicted enzyme activity range, from 150 to 975 U/g

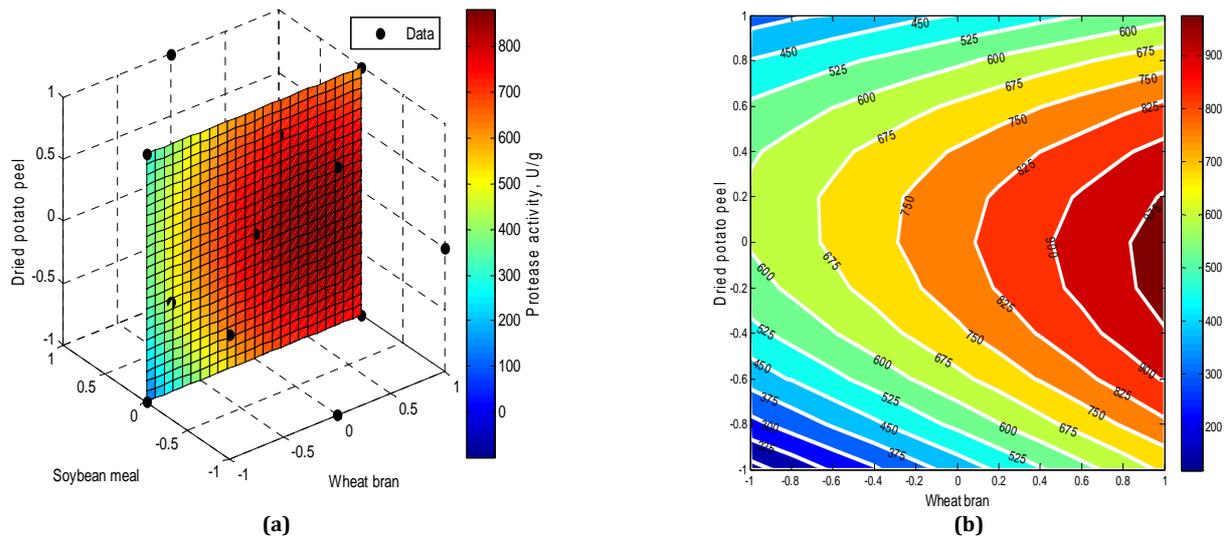


Fig. 5: Two-way interactions between wheat bran and DPP with soybean meal fixed at 3.75% w/w (a) Three dimensional plot and (b) Contour diagram with predicted enzyme activity range 150 to 975 U/g

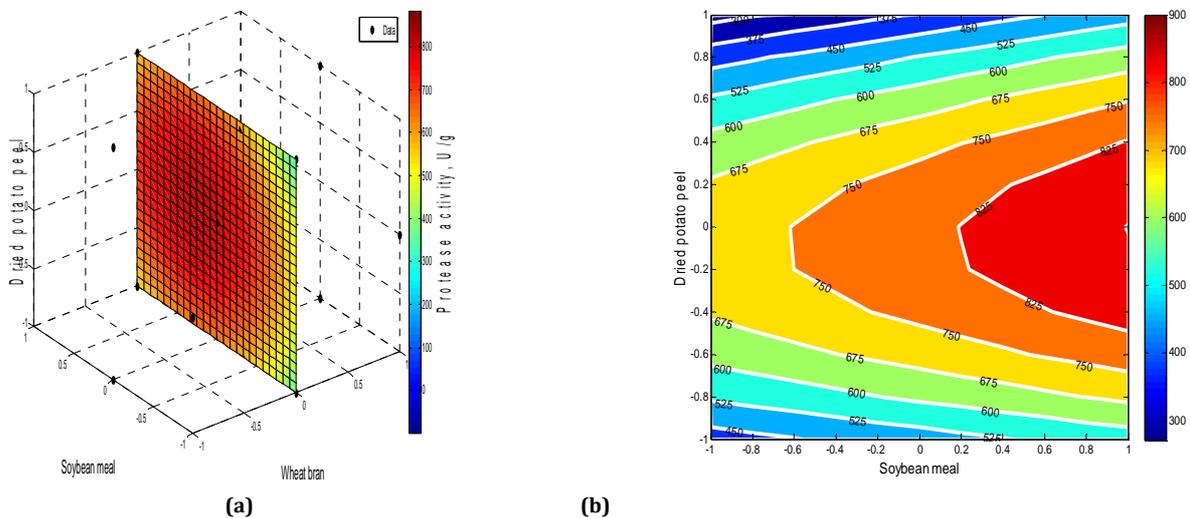


Fig. 6: Interactions between soybean meal and DPP with wheat bran at 7.5% (w/w) (a) 3-D plot and (b) Contour diagram with covered range of enzyme activity 450-825 U/g

Minimum to maximum predicted enzyme activity was noticed as 150 and 975 U/g from contour diagrams. Optimum combination of substrates (Wheat bran: 8.841 g, Soybean meal: 4.557 g, and DPP: 0.661 g) was achieved through predicted plot of full quadratic model ($p < 0.01$) with the acid protease activity of 817.83 U/g (± 44.047 U/g). The coefficients of second order polynomial model for the prediction of enzyme activity (table 4) and for biomass were determined by using ANOVA (Analysis of variance) and the proposed models were as follows:

Predicted acid protease activity:

$$Y_{\text{Protease activity}} = 807.83 + 219.04 X_1 + 87.46 X_2 - 13.55 X_3 // \text{linear effects} \\ + 29.37 X_1 X_2 - 83.42 X_1 X_3 + 19.24 X_2 X_3 // \text{Interactive effects} \\ - 208.573 X_1^2 - 200.525 X_2^2 - 169.52 X_3^2 // \text{Quadratic effects (9)}$$

Predicted mass of *Aspergillus* spp.:

$$Y_{\text{Biomass}} = 1.393 + 0.348 X_1 + 0.129 X_2 - 0.026 X_3 // \text{linear effects} \\ + 0.068 X_1 X_2 - 0.151 X_1 X_3 + 0.031 X_2 X_3 // \text{Interactive effects} \\ - 0.418 X_1^2 - 0.363 X_2^2 - 0.278 X_3^2 // \text{Quadratic effects (10)}$$

Multivariate analysis (table 4) highlighted that linear variables such as wheat bran X_1 , and soybean meal X_2 were significant ($*P < 0.01$) while an additional carbon source, DPP, X_3 ($*P < 0.01$) was shown to be less impact on enzyme production.

Key outcome from two-way interactions was cooperation between carbon sources, $X_1 X_3$, for growth as well as enzyme production ($*P < 0.05$) (Fig.5b). All three quadratic effects: X_1^2 , X_2^2 , X_3^2 ($*P < 0.01$) were significant and negative coefficients had indicated that higher levels of X_1 , X_2 , X_3 would reduce response. Computed F-value (Fisher's Statistical Test: 29.26) from ANOVA table (table 5) was an indication of better fitness of polynomial model to experimental data from design matrix ($P < 0.001$) (table 3). Multiple correlation coefficient (R^2 : 99.06%) had enlighten that the second order polynomial model could explain 99.06% of variability in the response and only 0.094% of the total variations were not explained by the model. Variations in predicted R^2 (98.13%) was corrected by adjusted R^2 (94.78%), both were suggesting a high significance model used for analyzing the data. The predicted results of RSM were confirmed by experimental verification. For this, fermentation was carried out with the above mentioned optimized medium and resultant response of fermentation was observed as 815.279 U/g (± 12.48 U/g) which was in accordance with predicted value.

Table 4: Results of regression analysis of the second order polynomial model with MATLAB (R2012a)

	Terms	Coefficient	Standard error	P value
Intercept	-	807.83	32.60	<0.01 (Significant)
Wheat bran (X_1)	Linear term	219.04	19.96	<0.01 (Significant)
Soybean meal (X_2)		87.46	19.96	<0.01 (Significant)
Dried potato peel (X_3)		-13.55	19.96	0.527
X_1X_2	Interaction terms	29.37	28.23	0.345
X_1X_3		-83.42	28.23	0.031
X_2X_3		19.24	28.23	0.525
X_1^2	Quadratic terms	-208.57	29.38	<0.01 (Significant)
X_2^2		-200.52	29.38	<0.01 (Significant)
X_3^2		-169.52	29.38	<0.01 (Significant)

Summary of ANOVA for biomass was given in table 6 which indicated that biomass concentration was well described by proposed polynomial model given in Eq.10 (F-Value: 36.612).

Table 5: Analysis of variance for the fitted second order regression model for acid protease activity (MS Excel-7)

	Df (Degrees of freedom)	SS(Sum of squares)	MS(Mean of squares)	F(Fischer's test value)	P value (Probability value)
Regression	9	839807.91	93311.99	29.25	0.0008
Residual	5	15945.74	3189.15		
Total	14	855753.60			

Table 6: Analysis of variance for the fitted second order regression model-Growth of *Aspergillus* spp

	Df (Degrees of freedom)	SS (Sum of squares)	MS (Mean of squares)	F(Fischer's test value)	P value (Probability value)
Regression	9	2.460	0.273	36.612	0.0005
Residual	5	0.037	0.007		
Total	14	2.497			

Multiple R: 99.25%; R^2_{Pre} : 98.50; R^2_{adj} : 95.81

Some of the previous studies used similar approach of sequential steps of PBD followed by RSM for optimization of both acid and alkaline proteases production from various microbial sources [6, 7, 26-30]. Acid protease activity from *Aspergillus niger* reported in present study was comparable with earlier studies of [4 (2500 U/l), 7 (183.13 U/ml), 25 (577 U/ml), 31 (148.28 U/g)]. However, the highest acid protease activity of 8.93×10^5 U/g from *Aspergillus oryzae* from wheat bran was achieved by [6]. Ligno-cellulosic materials, wheat bran and DPP were evaluated as carbon sources for the maximum yield of acid protease in the current study. Similarly, previous report [31] revealed that agro industrial waste, sugarcane bagasse, was a suitable substrate for alkaline protease from *Bacillus* spp. through statistical method. In addition, another study [32] have reported that agro residues/wastes can be utilized as low cost materials for production of enzymes, biofuel, organic and amino acids there by environmental pollution is reduced. On the same traits, corncobs and coffee pulp waste were tested for alkaline protease optimization by BBD and observed the maximum yield of 920 U/ml [33].

Nitrogen source plays an important role in the production of protease. Therefore, the present study revealed that soybean meal was proved to be the potential nitrogen source. Similarly, protease production media were designed with sole nitrogen source, peptone, and other factors (pH and moisture content) and achieved an

enzyme activity of 94.30 U/ml from *Penicillium citrinum*, isolated from fermented fish sauce [29].

Partial casein inhibition kinetics

In the present work we obtained maximum yield of enzyme through RSM method. Further study was carried out to achieve better yield with casein as assay substrate. In order to find out of suitable concentration of substrate on protease activity, the effect of substrate concentration in a range of 0.1 to 2.2 mmol was studied. The velocity of caseinolysis by crude acid protease was shown by Michaelis-Menten plot (fig. 7a) and Line weaver-Burk plot (Fig.7b). It was noticed that velocity had deviated from normal rectangular hyperbola to decreased pattern at excess casein and it was due to partial SI. Experimental velocity of casein hydrolysis reached to a maximum velocity of 5.956 μ M/s when casein concentration range is 0 to 0.4 mmol and then reduced to 2.89 μ M/s beyond 0.4 mmol. It was also noticed that a linear increase in velocity up to 0.4 mmol of casein concentration and an immediate decrease in velocity was observed till 1.1 mmol of concentration. Later the velocity reached to a steady value even the increase in substrate concentration (fig. 7a). Similar behavior for phosphofructokinase was observed [18] and the authors were described this trend was due to partial SI. In addition, the biological significance of SI was well illustrated for various biocatalysts [16].

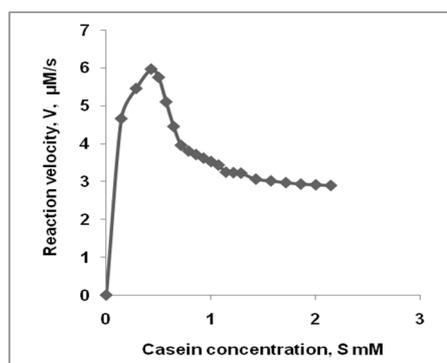


Fig. 7a: Plot showing the dependency of velocity on S-Deviation from rectangular behavior represented by Michaelis-Menten plot

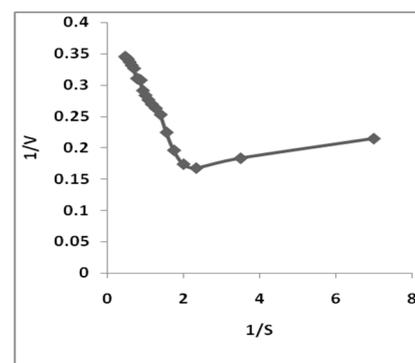


Fig. 7b: Display of non-linear behavior by Lineweaver-Burk plot

As mathematical models of normal competitive, non-competitive, and uncompetitive inhibition kinetics will not fit to present study, another simple proposed model of [18] and Andrew's model were employed to explain the impact of SI on enzyme velocity. For this purpose, a plot of $1/V$ vs. $1/S$ at lower casein (fig. 8) was used to calculate V_{max} and

dissociation constant for ES complex, K_1 , from its slope and intercept as $6.849 \mu\text{M/s}$ and 0.062 mmol . At lower casein amounts, substrate (S) binds to the active site of acid protease (E) forms ES. Without inhibition, complex ES dissociates into product (P) with lower concentrations of casein and theoretical V_{max} was obtained (Eq.3 and Eq. 4).

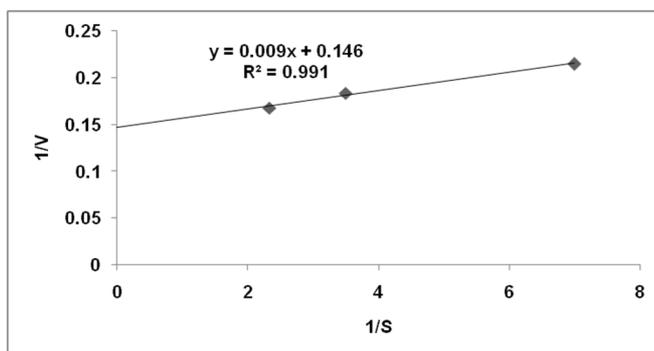


Fig. 8: Normal trend of double reciprocal graph for calculation on maximum velocity of reaction at lower concentrations of casein (V_{max} : $6.849 \mu\text{M/s}$ and $K_1 = 0.062 \text{ mmol}$)

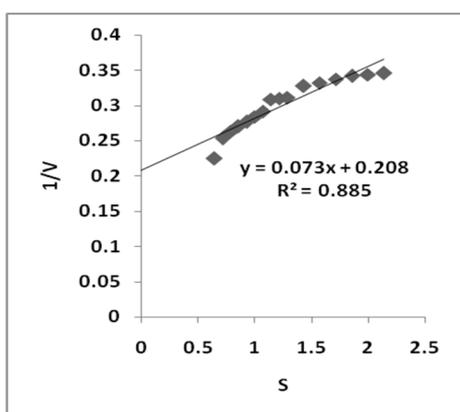


Fig. 9a: Plot of variation of reaction velocity with higher casein concentration (Model1: V_{max} : $4.807 \mu\text{M/s}$ and Dissociation constant for SES $K_N = 2.849 \text{ mmol}$)

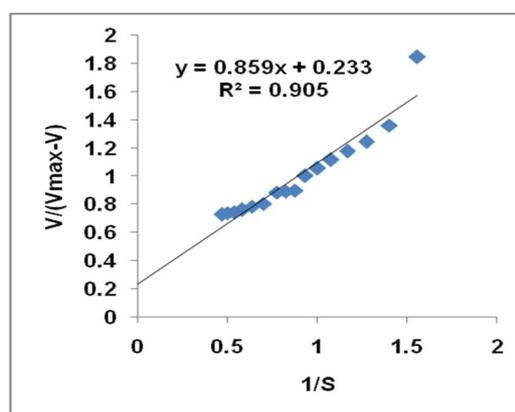


Fig. 9b: Display of velocity ratio as function of inverse higher casein concentration (Model 2 Rate constant ratio, k_4/k_2 , from intercept was 0.233 and Dissociation constant for SES, K_N from slope = 0.659 mmol)

The most important parameter for SI was determination of dissociation constant for SES complex, K_N which was found to be 2.849 mmol (Fig.9a-Model 1) and the same was 0.659 mmol . (Fig.9b-Model 2). It was understood that both above mentioned models were satisfactory to explain the modeling of SI. It was understood that promised value of K_N at higher substrate concentration was explained the role of SES complex on enzyme velocity. Same effect was shown of substrate inhibition (Eq. 3), excess amount of casein further binds to complex ES then forms more complicated complex SES. Especially in partial substrate inhibition, dissociation of this complex is much slower than ES complex and reduces the velocity of reaction. This was confirmed with reduced V_{max} from: 6.849 (Fig.8) to $4.807 \mu\text{M/s}$ (fig. 9a). Further reaction rate constant ratio k_4/k_2 , was computed as 0.233 from the intercept of $V/(V_{max}-V)$ vs. $1/S$ (Fig.9b). Rate constant ratio for partial SI must be less than 1 ($k_4/k_2 < 1$) [18]. Reported value of k_4/k_2 had confirmed that velocity of hydrolysis of casein was inhibited by partial casein inhibition. Model 2 was the better fit to experimental data reaction rate with casein as R^2 : 90.5% (fig. 9b). Enzymatic kinetic studies were performed for detergent-compatible protease from *Aspergillus terreus* and reported kinetic parameters were V_{max} : 12.8 U/ml and K_m of 5.4 mg/ml [34].

CONCLUSION

Present study had revealed that the statistical methodology could be adopted easily for the design of suitable medium for the optimal production of acid protease with low cost substrates in SSF against

OVAT. PBD had allowed the quick identification of significant solid substrates and BBD determined the combination of carbon and nitrogen supplements for better protease activity in simple experiments. The experimental data of RSM was best fit to predicted quadratic model. Kinetic studies on partial casein inhibition were understood with simple reaction mechanisms. Both above mention models of SI were very useful in understanding of deviation of rate of enzymatic reaction with substrate. Calculation of inhibitory constant, K_N and rate constant ratio (k_4/k_2) was more useful in substrate inhibition.

ABBREVIATION

ANOVA: Analysis of variance, BBD: Box Behnken design, DPP: Dried potato peel, OVAT: One variable at a time, PBD: PlackettBurman design, RSM: Response Surface Methodology, R^2_{adj} : Adjusted R square, R^2_{pre} : Predicted R square, Spp.: Species, SSF: Solid state fermentation

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AUTHORS CONTRIBUTIONS

Radha Seela¹: Carried out the Research work.

Narasimha Golla²: Provided guidance, critical review, revision and corresponding this article.

Sridevi Ayla: Helped while caring the experiments.

Prasad NBL: Co-supervisor of this work.

CONFLICT OF INTERESTS

The authors declare that they have no conflict of interest

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